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The theory and application of Navier-Stokeslets (NSlets)

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Consider a closed body moving in an unbounded fluid that decays to rest in the far-field and governed by the incompressible Navier-Stokes equations. By considering a translating reference frame, this is equivalent to a uniform flow past the body. A velocity representation is given as an integral distribution of Green's functions of the Navier-Stokes equations which we shall call NSlets. The strength of the NSlets is the same as the force distribution over the body boundary. An expansion for the NSlet is given with the leading-order term being the Oseenlet. To test the theory, the following three two-dimensional steady flow benchmark applications are considered. First, consider uniform flow past a circular cylinder for three cases: low Reynolds number; high Reynolds number; and also intermediate Reynolds numbers at values 26 and 36. These values are chosen because the flow is still steady and hasn't yet become unsteady. For low Reynolds number, approximate the NSlet by the leading order Oseenlet term. For high Reynolds number, approximate the NSlet by the Eulerlet which is the leading order Oseenlet in the high Reynolds number limit. For the intermediate Reynolds numbers, approximate the NSlet by an Eulerlet close to its origin, and an Oseenlet further away. Second, consider uniform flow past a slender body with elliptical cross-section with Reynolds number $Re \sim 10^6$, and approximate the NSlet by the Eulerlet. Finally, consider the Blasius problem of uniform flow past a semi-infinite flat plate and consider the first three terms in the NSlet approximation.

Keywords: Navier-Stokes equations, NSlets.

I. INTRODUCTION

A Boundary Integral velocity representation is derived for the Navier-Stokes equations in terms of their Green's functions, called NSlets, for a body in an exterior-domain uniform flow. This result is already known for the steady case¹, where it is assumed that the Boundary Integral representations around the fluid point and the body can be represented by domain integrations involving Dirac delta functions. In this paper, these assumptions shall not be made and, instead, the Boundary Integral representations shall be evaluated directly. Furthermore, the representation is extended to include time dependent as well as steady flow.

The result is a generalization of existing results in the literature for Stokes^{2,3}, Oseen⁴ and Euler⁵ models. These represent the flow by an integral distribution over the body boundary of their respective Green's functions which have a strength given by the force distribution. In the low Reynolds number limit the NSlet tends to the Stokeslet, in the high Reynolds number limit the NSlet tends to the Eulerlet, and in the far-field the NSlet tends to the Oseenlet. In this way, the new formulation is seen to reduce to existing formulations. For the Stokes and Oseen flow the Boundary Integral representation in terms of Stokeslets and Oseenlets, respectively, is well-known in the literature as the equations are linear²⁻⁴. However, the result for Euler flow by using Eulerlets is significant as it gives a Green's integral representation for the velocity of the non-linear Euler equations⁵. A theoretical argument was then given for Navier-Stokes flow by using NSlets¹, but this argument assumed the use of Dirac delta function representations of the domain integrations rather than the boundary integrations, and was also restricted to the steady case only.

In the present paper, this assumption is not made, and instead we look to evaluate the Boundary Integrals rather than the delta function domain integrals in the Green's integral representation. To evaluate the integration around the fluid point, we note that a moving reference frame translating with the velocity of the fluid point will in the vicinity of the point have vanishingly small fluid velocity and so be represented by a linear Stokes flow. The non-linearity in the Eulerian Navier-Stokes description begins to disappear and approach the Lagrangian representation following a fluid particle in the vicinity of the point where the Lagrangian and Eulerian representations approach each other. Similarly, the far-field integration will be represented by an Oseen flow. This means that over both these integrals, the flow becomes linear and the non-linear quadratic variation in the Navier-Stokes equations becomes negligible; in this way the integrals may be subsequently evaluated. This is also checked by determining the order of contribution from the non-linear variation and demonstrating that it is vanishingly small in the limit. Furthermore, the non-linear contribution in the Green's integral representation is shown to be represented by a potential defined by a line integration over a radial spoke emanating from the fluid point. By considering the interior as well as exterior problem, we see that this potential is continuous over the body domain boundary as we cross from the exterior to the interior domain. Consequently, the non-linear contributions from the exterior and the interior domains cancel, yielding a velocity representation by a linear integral distribution of NSlets only.

We give a representation of the NSlet by an infinite series expansion with the first term being the Oseenlet. In this way, the theory is tested on three benchmark problems.

First, consider uniform flow past a circular cylinder for three cases: low, high and intermediate Reynolds number. For low Reynolds number approaching unity, it is shown that the drag coefficient is closer to experiment than

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Symbol	Definition
ρ, μ, U, l, T	Dimensional parameter: density, coefficient of viscosity, uniform stream velocity, typical body length, typical time period
$Re = \rho Ul / \mu$	Dimensionless Reynolds number
$St = l / (UT)$	Dimensionless Strouhal number
Superscript \dagger $\mathbf{u}^\dagger, p^\dagger, \mathbf{x}^\dagger$	Dimensional variable: Navier-Stokes velocity, pressure and position vector
\mathbf{u}, p	Dimensionless Navier-Stokes velocity and pressure perturbed to a uniform stream
\mathbf{v}	Dimensionless Boundary Layer velocity perturbed to a uniform stream
\mathbf{x}	Dimensionless position vector
\mathbf{x}'	Variable of integration in the Green's integral of the dimensionless position vector
r	Dimensionless radial length in two dimensions
r^*	Dimensionless length in two dimensional space-time
R	Dimensionless radial length in three dimensions
R^*	Dimensionless length in three dimensional space-time
a_j	Vector representation with index starting from 1 and ending at dimension of space
a_J	Vector representation with index starting from 0 with a_0 the time co-ordinate
$a_{.i}$	Differentiation of a with respect to x_i
$a_{.i}$	Differentiation of a with respect to x'_i
Q_k	Non-linear quadratic term in Green's integral
q_{jk}	Potential of Q_k
$\Sigma, d\Sigma,$ $\partial\Sigma,$ $d\sigma$	A region of space, an element of the space, the boundary of the region of space, an element of the boundary
δ	Dirac delta function
δ_{ij}	Kronecker delta

TABLE I: Nomenclature

the matched asymptotic method of Kaplun and Lagerstrom⁶ where Kaplun's result is given by Yano and Kieda⁷. For high Reynolds number, the NSlet is approximated by the Eulerlet which is the leading order Oseenlet in the high Reynolds number limit; refer to the results of Chadwick⁵ which show good agreement with experiment for laminar and turbulent flows. There have been several recent studies on flow past cylinders such as oscillations of cylinders⁸ and their stable modes⁹, the vortex motion above a plane¹⁰ and an experimental Partial Image Velocimetry (PIV) investigation with dual step cylinders¹¹. Similarly, the focus of this application is circular cylinders with the emphasis on the mean-steady flow to use as a benchmark test. For intermediate Reynolds number at values 26 and 36, the NSlet is approximated by an Eulerlet close to its origin, and an Oseenlet further away. This reduces to the matched method of Chadwick¹² which shows good comparison to experiment.

Second, consider uniform flow with Reynolds number $Re \sim 10^6$ past a slender body whose cross-section is elliptical, and approximate the NSlet by the Eulerlet. It is seen that this is equivalent⁵ to the uniform flow past a slender body with elliptical cross-section in Oseen flow given by Chadwick¹³ who

satisfies the slip body boundary condition for the potential part of the Oseen flow description.

Finally, consider the Blasius problem of uniform flow past a semi-infinite flat plate and take the first three terms in the NSlet expansion. The first of these terms reduces to the Oseen-Blasius solution, which does not predict well the Blasius boundary layer. However, including the next two terms is equivalent to the expansion obtained from a different approach by Kusunaka¹⁴. In this way, we see that with each term the Blasius solution is recovered more accurately and the first three terms in the NSlet are sufficient to give a good approximation.

II. STATEMENT OF THE PROBLEM

We consider time-dependent, incompressible fluid of density ρ and viscosity μ such that the Navier-Stokes equation

$$\rho \frac{\partial u_i^\dagger}{\partial t^\dagger} + \rho u_j^\dagger \frac{\partial u_i^\dagger}{\partial x_j^\dagger} = -\frac{\partial p^\dagger}{\partial x_i^\dagger} + \mu \frac{\partial^2 u_i^\dagger}{\partial x_j^\dagger \partial x_j^\dagger} \quad (1)$$

and continuity equation

$$\frac{\partial u_i^\dagger}{\partial x_i^\dagger} = 0 \quad (2)$$

hold throughout the fluid, where the symbol \dagger denotes dimensional and unperturbed quantities. Fields u_i^\dagger and p^\dagger are the fluid velocity and static pressure respectively, in Cartesian co-ordinates x_i^\dagger , $1 \leq i \leq 2$ for two-dimensional flow and $1 \leq i \leq 3$ for three-dimensional flow. Einstein's convention of a repeated suffix implying a summation is used ($a_i b_i = a_1 b_1 + a_2 b_2 + a_3 b_3$ in three-dimensions, for example.)

Consider an exterior problem with a uniform velocity translation such that the far-field boundary condition has the fluid tending towards a uniform stream of magnitude U aligned along the x_1^\dagger axis such that

$$u_i^\dagger = U \delta_{i1}, \quad (3)$$

where δ_{ij} is Kronecker delta such that $\delta_{ij} = 1$ when $i = j$ and $\delta_{ij} = 0$ otherwise. The normalized perturbed velocity u_i and (Bernoulli) normalized perturbed pressure p to the uniform stream satisfy $u_i^\dagger = U \delta_{i1} + U u_i$, $p^\dagger = -(1/2)\rho U^2 + \rho U^2 p$ and the normalized co-ordinates are $x'_i = l x_i^\dagger$, $t' = T t^\dagger$. The perturbed Navier-Stokes equation is then

$$St \frac{\partial u_i}{\partial t'} + \frac{\partial u_i}{\partial x'_1} + u_j \frac{\partial u_i}{\partial x'_j} = -\frac{\partial p}{\partial x'_i} + (1/Re) \frac{\partial^2 u_i}{\partial x'_j \partial x'_j}, \quad (4)$$

where $St = l / (UT)$ is the Strouhal number and $Re = \rho Ul / \mu$ is the Reynolds number. We can rewrite (4) as

$$N_i = St u_{i;0} + u_{i;1} + u_j u_{i;j} + p_{;i} - (1/Re) u_{i;jj} = 0 \quad (5)$$

where the semi-colon represents a derivative with respect to the primed co-ordinates and a derivative with respect to the

index 0 means a derivative with respect to time t' ($a_{:,0} = \frac{\partial a}{\partial t'}$, for example.) In (5), it is implicitly assumed that the velocity and pressure are functions of the primed co-ordinates (t', x'_i) . In the Green's Boundary Integral formulation, we denote the variable of integration by the primed co-ordinates. By contrast, the Green's function depends on the variables $(t - t', x_i - x'_i)$, where the co-ordinate of a point in the fluid is given as (t, x_i) . Thus, we can designate the k th NSlet for the velocity as $u_{ik}(t - t', x_i - x'_i)$ and the pressure as $p_k(t - t', x_i - x'_i)$ such that the following equation is satisfied:

$$N_{ik} = St u_{ik,0} + u_{ik,1} + u_{jk^*} u_{ik^*,j} + p_{k,i} - (1/Re) u_{ik,jj} = -\delta \delta_{ik}. \quad (6)$$

Here, a comma denotes a derivative with respect to the unprimed co-ordinates (implying $a_{:,j} = -a_{,j}$) and the asterix means no implied summation ($a_{k^*} a_{k^*} = a_1 a_1$ when $k = 1$, for example). The symbol δ denotes the Dirac delta function such that $\int_{\Sigma_\delta} \delta d\Sigma = 1$ where the domain Σ_δ is sufficiently close to and encloses the origin.

Consider the domain Σ in space-time consisting of an exterior domain Σ_+ and interior domain Σ_- to the closed boundary $\partial\Sigma_0$ over which the velocity is specified. This closed boundary could represent a body in a fluid. Further, consider the exterior domain Σ_+ to be bounded by a vanishingly small boundary $\partial\Sigma_\delta$ around the point (t, x_i) , and a far-field boundary $\partial\Sigma_\infty$. The Green's integration over (t', x'_i) will be taken over the whole of the domain Σ as shown in Figure 1.

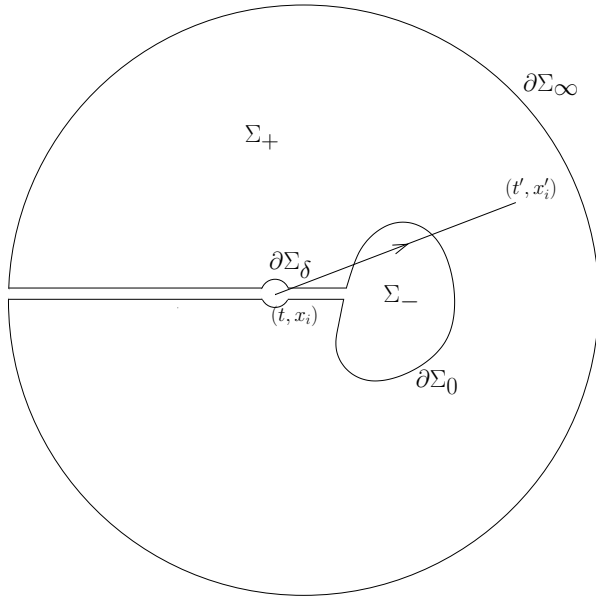


FIG. 1: The domain of integration Σ and its boundaries

Over the far-field boundary $\partial\Sigma_\infty$ we have

$$u_i \rightarrow 0. \quad (7)$$

In addition, the NSlet satisfies

$$\begin{aligned} \int_{\Sigma_\delta} N_{ik} d\Sigma &= \int_{\Sigma_\delta} N_{iJk,J} d\Sigma = \int_{\partial\Sigma_\delta} N_{iJk} n_J d\sigma \\ &= - \int_{\Sigma_\delta} \delta \delta_{ik} d\Sigma = -\delta_{ik} \end{aligned} \quad (8)$$

where

$$N_{iJk} = St u_{ik} \delta_{0J} + u_i \delta_{1J} + u_{jk^*} u_{ik^*} + p_k \delta_{ij} - (1/Re) u_{ik,j} \quad (9)$$

where σ refers to the boundary of the space Σ and $d\sigma$ is an infinitesimal element on the boundary of the space Σ . The capital index J is for space-time $0 \leq J \leq 3$ in the case of 3-dimensional flow, and $J = 0$ refers to time. The space vector $a_j = (a_1, a_2, a_3)$ may now be represented in space-time by $a_J = (a_0, a_1, a_2, a_3)$ where $a_0 = 0$. Therefore, the complementary conjugate integration over primed space is

$$\begin{aligned} \int_{\Sigma_\delta} N_{ik} d\Sigma &= \int_{\Sigma_\delta} N_{ik} d\Sigma' = \int_{\Sigma_\delta} N_{iJk,J} d\Sigma' \\ &= - \int_{\Sigma_\delta} N_{iJk,J} d\Sigma' = - \int_{\partial\Sigma_\delta} N_{iJk} n_J d\sigma', \end{aligned} \quad (10)$$

and so

$$\int_{\partial\Sigma_\delta} N_{iJk} n_J d\sigma' = \delta_{ik}. \quad (11)$$

III. GREEN'S INTEGRAL FORMULATION

Consider the Green's integral formulation of Oseen¹⁵:

$$\int_{\Sigma} [N_i u_{ik} - N_{ik} u_i] d\Sigma' = 0. \quad (12)$$

The integrand is reformulated as

$$\begin{aligned} N_i u_{ik} - N_{ik} u_i &= (St u_{i,0} + u_{i,1} + u_j u_{i,j} + p_{:,i} - (1/Re) u_{i,jj}) u_{ik} \\ &\quad - (St u_{ik,0} + u_{ik,1} + u_{jk^*} u_{ik^*,j} + p_{k,i} - (1/Re) u_{i,jj}) u_i \\ &= [St u_i u_{ik}]_{:,0} + [u_i u_{ik}]_{:,1} + [p u_{ik} + p_k u_i]_{:,i} \\ &\quad - (1/Re) [u_{i,j} u_{ik} - u_{ik,j} u_i]_{:,j} + [u_{jk^*} u_{ik^*} u_i]_{:,j} + Q_k, \end{aligned} \quad (13)$$

where the non-linear term is

$$Q_k = u_j u_{i,j} u_{ik} - u_{i,j} u_{jk^*} u_{ik^*}. \quad (14)$$

It follows that Q_k may be represented by a potential q_{jk} such that $q_{jk,j} = Q_k$, where

$$q_{jk} = q_k \hat{r}_j = q_k \cos \theta_j. \quad (15)$$

\hat{r}_j is the unit radial vector in the direction of x'_i from x_i , and $\cos \theta_j = (x'_j - x_j)/r$ with $r = \sqrt{(x'_1 - x_1)^2 + (x'_2 - x_2)^2}$ in two-dimensions, and $\cos \theta_j = (x'_j - x_j)/R$ with $R = \sqrt{(x'_1 - x_1)^2 + (x'_2 - x_2)^2 + (x'_3 - x_3)^2}$ in three-dimensions.

A. Definition of q_k

We define q_k as a line integral along a radial spoke such that

$$q_k = \begin{cases} (1/r) \int_0^r r' Q'_k dr', & \text{in two-dimensions} \\ (1/R^2) \int_0^R R'^2 Q'_k dR', & \text{in three-dimensions.} \end{cases} \quad (16)$$

Hence $N_i u_{ik} - N_{ik} u_i = n_{S_{Jk;J}}$, where

$$\begin{aligned} n_{S_{Jk}} &= S t u_i u_{ik} \delta_{j0} + u_i u_{ik} \delta_{j1} + [p u_{ik} + p_k u_i] \delta_{ij} \\ &\quad - (1/Re) [u_{i;j} u_{ik} - u_{ik;j} u_i] + u_{jk} u_{ik} u_i + q_{jk} \\ &= u_i [S t u_{ik} \delta_{j0} + u_{ik} \delta_{j1} + u_{jk} u_{ik} + p_k \delta_{ij} \\ &\quad - (1/Re) u_{ik;j}] - u_{ik} [-p \delta_{ij} + (1/Re) u_{i;j}] + q_{jk} \\ &= u_i N_{iJk} - u_{ik} \tau_{ij} + q_{jk}, \end{aligned} \quad (17)$$

and $\tau_{ij} = -p \delta_{ij} + (1/Re) u_{i;j}$ is the stress tensor. So we have

$$\begin{aligned} \int_{\Sigma} [N_i u_{ik} - N_{ik} u_i] d\Sigma' &= \int_{\Sigma} n_{S_{Jk;J}} d\Sigma' = \int_{\partial\Sigma} n_{S_{Jk}} n_j^\Sigma d\sigma', \\ &= \int_{\partial\Sigma} [u_i N_{iJk} - u_{ik} \tau_{ij} + q_{jk}] n_j^\Sigma d\sigma', \end{aligned} \quad (18)$$

where n_j^Σ is the outward pointing normal to the domain Σ .

B. Evaluation around $\partial\Sigma_\delta$

Consider translating with the velocity at x_i , then the Stokes equation holds in the vicinity of x_i represented by the Stokeslets. Equivalently, one might consider that the velocity is, to leading order, the velocity at the fluid point. So locally, the Oseen linearization about this velocity holds, giving the Oseen equations in the vicinity of x_i represented by the Oseenlets. Sufficiently close to the point, the Oseenlets tend toward the Stokeslets. The NSlet will thus have the same order of magnitude as the Stokeslet in the vicinity of the point. The Stokeslets have order¹⁵

$$u_{ik} \sim \begin{cases} \ln r, & \text{in two-dimensional steady flow} \\ 1/R, & \text{in three-dimensional steady flow} \\ 1/r^*, & \text{in two-dimensional unsteady flow} \\ 1/(R^* \sqrt{R^*}), & \text{in three-dimensional unsteady flow} \end{cases} \quad (19)$$

where $r^* = \sqrt{(t-t')^2 + r^2}$ and $R^* = \sqrt{(t-t')^2 + R^2}$ are the space-time distance measures for two-dimensional and three dimensional flows respectively. The orders for the quadratic variation are then

$$Q_k \sim \begin{cases} (\ln r)^2 \\ 1/R^2 \\ 1/r^{*2} \\ 1/(R^{*3}) \end{cases} \quad q \sim \begin{cases} r(\ln r)^2 \\ 1/R \\ 1/r^* \\ 1/(R^{*2}) \end{cases} \quad (20)$$

for two-dimensional steady, three-dimensional steady, two-dimensional unsteady and three-dimensional unsteady flows,

respectively. This leads to the integral contributions

$$\int_{\partial\Sigma_\delta} u_{ik} d\sigma' \sim \begin{cases} r \ln r \rightarrow 0 \\ R^2/R = R \rightarrow 0 \\ r^{*2}/r^* = r^* \rightarrow 0 \\ R^{*3}/(R^* \sqrt{R^*}) = R^{*3/2} \rightarrow 0 \end{cases} \quad (21)$$

$$\int_{\partial\Sigma_\delta} q d\sigma' \sim \begin{cases} (r \ln r)^2 \rightarrow 0 \\ R^2/R = R \rightarrow 0 \\ r^{*2}/r^* = r^* \rightarrow 0 \\ R^{*3}/(R^{*2} = R^* \rightarrow 0. \end{cases} \quad (22)$$

So, the only non-zero contribution to the evaluation around $\partial\Sigma_\delta$ comes from

$$\begin{aligned} \int_{\partial\Sigma_\delta} u_i N_{iJk} n_j^\Sigma d\sigma' &= u_i \int_{\partial\Sigma_\delta} N_{iJk} n_j^\Sigma d\sigma' \\ &= -u_i \int_{\partial\Sigma_\delta} N_{iJk} n_j d\sigma' \\ &= -u_i \delta_{ik} \\ &= -u_k. \end{aligned} \quad (23)$$

C. Evaluation around $\partial\Sigma_\infty$

In the far-field, the Navier-Stokes equation tends toward the Oseen equation and, accordingly, the NSlets tend towards the Oseenlets; it is known that this far-field integral is zero (see for example¹⁶ for the three-dimensional steady case). Equivalently, the only difference in integrands between the Navier-Stokes and Oseen representations is the non-linear quadratic velocity contribution, which decays faster than the velocity contribution. Since the velocity contribution decays to zero, then the non-linear contribution must do so as well.

D. Velocity representation

Putting these results into (18) whilst noting that u_i, N_{iJk} and q_{jk} are all continuous across the body boundary $\partial\Sigma_0$ whereas τ_{ij} is not necessarily, gives a representation for the fluid velocity as

$$\begin{aligned} u_k &= \int_{\partial\Sigma_0} [u_i N_{iJk} - u_{ik} \tau_{ij} + q_{jk}]^+ n_j^\Sigma d\sigma' \\ &\quad + \int_{\partial\Sigma_0} [u_i N_{iJk} - u_{ik} \tau_{ij} + q_{jk}]^- n_j^\Sigma d\sigma' \\ &= \int_{\partial\Sigma_0} -[u_i N_{iJk} - u_{ik} \tau_{ij} + q_{jk}]^+ n_j d\sigma' \\ &\quad + \int_{\partial\Sigma_0} [u_i N_{iJk} - u_{ik} \tau_{ij} + q_{jk}]^- n_j d\sigma' \\ &= \int_{\partial\Sigma_0} [\tau_{ij}^+ - \tau_{ij}^-] u_{ik} n_j d\sigma' \\ &= \int_{\partial\Sigma_0} F_i u_{ik} d\sigma', \end{aligned} \quad (24)$$

where $[\dots]^+$ means the evaluation in the exterior domain, $[\dots]^-$ means the evaluation in the interior domain, and $F_i = [\tau_{ij}^+ - \tau_{ij}^-]n_j$. For the steady case, $\partial\Sigma_0$ is the body boundary which we denote by $\partial\Sigma_B$, and so

$$u_k = \int_{\partial\Sigma_B} F_i u_{ik} d\sigma'. \quad (25)$$

Writing out the function arguments in full, the vector position is given as $\mathbf{x} = (x_1, x_2, x_3)$ in three-dimensions for example, and so (25) is

$$u_k(\mathbf{x}) = \int_{\partial\Sigma_B} F_i(\mathbf{x}') u_{ik}(\mathbf{x} - \mathbf{x}') d\sigma'. \quad (26)$$

This means that the velocity is represented by a Boundary Integral distribution of NSlets positioned over the body surface, $\partial\Sigma_B$ with strength $F_i(\mathbf{x}')$ for a point $\mathbf{x}' = (x'_1, x'_2, x'_3)$ on $\partial\Sigma_B$. Since the body boundary conditions are given in terms of the velocity on $\partial\Sigma_B$, the general problem is solved in terms of a Boundary Integral representation and discretized by a numerical scheme such as the Boundary Element Method.

For the unsteady case, $\partial\Sigma_0$ is the space-time boundary which is the body boundary traced out over time and so

$$\begin{aligned} u_k &= \int_{-\infty}^t \left\{ \int_{\partial\Sigma_B} F_i u_{ik} d\sigma' \right\} dt' \\ &= u_k|_{t=0} + \int_0^t \left\{ \int_{\partial\Sigma_B} F_i u_{ik} d\sigma' \right\} dt' \end{aligned} \quad (27)$$

where $u_k|_{t=0}$ is the velocity field at time $t = 0$. Writing out the function arguments in full, now including time t and space \mathbf{x} as (t, \mathbf{x}) , then equation (27) is

$$\begin{aligned} u_k(t, \mathbf{x}) &= u_k(0, \mathbf{x}) \\ &+ \int_0^t \left\{ \int_{\partial\Sigma_B} F_i(t', \mathbf{x}') u_{ik}(t - t', \mathbf{x} - \mathbf{x}') d\sigma' \right\} dt'. \end{aligned} \quad (28)$$

This means that the velocity is represented by a Boundary Integral distribution of NSlets positioned over the body surface, $\partial\Sigma_B$ with strength $F_i(t', \mathbf{x}')$ for a point \mathbf{x}' on the body surface, traced out over time t' where $0 \leq t' \leq t$ from an initial condition given at time $t = 0$. Since the body boundary conditions are given in terms of the initial value at $t = 0$ and the subsequent body boundary position up to time t , then the general problem is solved in terms of a Boundary Integral representation, which can then be given by a numerical scheme such as the Boundary Element Method for the space variable and a Finite Difference Method for the time variable.

E. Pressure representation

Once the problem has been solved for the velocity, then the pressure can subsequently be obtained from the (generalized) Bernoulli equation in the following way. The fundamental theorem of vector calculus means that any vector can

be decomposed into a vorticity-free and potential-free part. So, we may write $u_i = \phi_{,i} + u_i^{\omega}$, where $\phi_{,i}$ is the vorticity-free part and u_i^{ω} is the potential-free part. A word of caution, this representation is equivalent to the Lamb-Goldstein velocity decomposition which has been shown by Chadwick¹⁷ not to necessarily hold everywhere in the field. However, this issue can be overcome by assuming an integral distribution of the Green's functions instead¹⁷, and this is what we assume here. Similarly, the expression for the fluid head can be written as $h_i = u_j u_{i,j} = h_{,i} + h_i^{\omega}$, where $h_{,i}$ is the vorticity-free part and h_i^{ω} is the potential-free part. Then, the pressure gradient, which is vorticity-free, is given by the vorticity-free components only in the Navier-Stokes equation (5). Integrating gives

$$p = -St\phi_{,0} - \phi_{,1} - h \quad (29)$$

since $\phi_{,jj} = 0$ from the continuity equation. In the inviscid Euler case, we have $h = (1/2)\phi_{,j}\phi_{,j}$ and so in this case the generalized Bernoulli equation (29) reduces to the standard Bernoulli equation. Instead in the viscous case the head h is also likely to include the viscous velocity.

IV. NSLET REPRESENTATION

We give an expansion for the NSlet, and then use this below to consider some benchmark applications. Far from the point (t, x_i) , the NSlets u_{ik} tend toward the Oseenlets u_{ik}^0 . So, in the far-field, the following asymptotic expansion is valid:

$$u_{ik} = u_{ik}^0 + u_{ik}^I + \dots \quad (30)$$

In the above equation, the Oseenlets u_{ik}^0 are known, see for example Oseen¹⁵, and satisfy the Oseenlet equation

$$u_{ik,0}^0 + u_{ik,1}^0 + u_{jk}^0 u_{ik^*,j}^0 + p_{k,i}^0 - (1/Re)u_{ik,jj}^0 = -\delta\delta_{ik}. \quad (31)$$

The next term in the expansion then satisfies

$$u_{ik,0}^I + u_{ik,1}^I + u_{jk}^I u_{ik^*,j}^I + p_{k,i}^I - (1/Re)u_{ik,jj}^I = -u_{jk}^0 u_{ik^*,j}^0, \quad (32)$$

and so on. In this way, we can expand asymptotically near to the point (t, x_i) , where the NSlets tend towards the Stokeslets. Since the Oseenlets tend towards the same Stokeslets, then the same expansion can be used to represent the expansion sufficiently close to the point. So sufficiently far away and sufficiently close to the point, the NSlets are represented by

$$u_{ik} = \sum_{N=0}^{N=\infty} u_{ik}^N. \quad (33)$$

This expression can then be used to continue for the NSlets into the remainder of the domain. In the applications that follow, we approximate the NSlet given in (33) in the following ways: for low Reynolds number we consider the first term in this expression only, which is the Oseenlet and which itself tends to the Stokeslet for low Reynolds number; for high Reynolds number, we consider the Eulerlet which is the high Reynolds number limit of the Oseenlet; for intermediate Reynolds number, we consider the NSlet approximated by

an Eulerlet in the near-field and Oseenlet in the far-field; and for boundary layer flow we consider the first three terms in the NSlet expansion and as well apply the boundary layer approximation.

V. APPLICATIONS

We consider three problems. The first flow past a circular cylinder across a variety of Reynolds numbers; the second flow past a slender body aligned closely to the flow direction at high Reynolds number with elliptical cross-section; the third, boundary layer flow past a semi-infinite flat plate.

A. Two-dimensional steady flow past a circular cylinder at low Reynolds number

1. Low Reynolds number flow

Consider using the velocity representation given by (25) in a Boundary Element numerical scheme such as presented by Dang and Chadwick¹⁸. In this scheme, the force distribution is approximated by shape functions located at n nodes on the body boundary such that

$$F_j \approx N_\beta F_{\beta j} \quad (34)$$

where $1 \leq \beta \leq n$, and the repeated index β implies a summation over all n terms. Under the standard Galerkin scheme, n weighting functions W_α are then considered giving the following equations to be solved:

$$\int_{\partial\Sigma_B} W_\alpha u_i d\sigma = \int_{\partial\Sigma_B} W_\alpha \int_{\partial\Sigma_B} N_\beta F_{\beta j} u_{ij} d\sigma' d\sigma \quad (35)$$

where $1 \leq \alpha \leq n$. So

$$u_{\alpha i} = u_{\alpha\beta ij} F_{\beta j}, \quad (36)$$

where $u_{\alpha i} = \int_{\partial\Sigma_B} W_\alpha u_i d\sigma$ and $u_{\alpha\beta ij} = \int_{\partial\Sigma_B} W_\alpha \int_{\partial\Sigma_B} N_\beta u_{ij} d\sigma'$. Renumbering $\alpha^* = \alpha + (i-1)n$ and $\beta^* = \beta + (j-1)n$ then gives the matrix equation

$$u_{\alpha^*} = u_{\alpha^*\beta^*} F_{\beta^*} \quad (37)$$

which can be solved by a dense matrix solver to determine an approximation for the force distribution F_i at each node β given by $F_{\beta i}$.

At low Reynolds number, the near-field flow tends towards Stokes flow and the far-field flow tends towards Oseen flow. To avoid the Stokes paradox, these two flows must be matched. We note that in the far-field the NSlets in (25) are approximated by the Oseenlets giving an Oseen flow field approximation in the field far from the body. It is also noted that in the near-field, the Oseenlet approximates to the Stokeslet, giving a Stokes flow field close to the body. Therefore, approximating the NSlets by the Oseenlets in (25) gives

$$u_k \approx u_k^0 = \int_{\partial\Sigma_B} F_i^0 u_{ik}^0 d\sigma'. \quad (38)$$

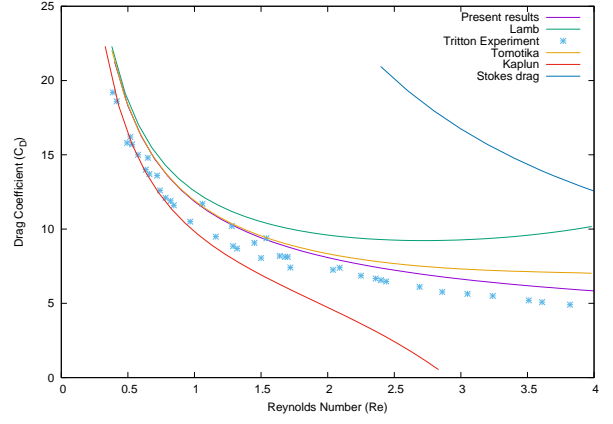


FIG. 2: Comparison of drag coefficient against Reynolds number¹⁸.

This is expected to give a good leading order approximation to the flow field from this theory where u_k^0 is the Oseen velocity approximation, F_i^0 is the force distribution for the two-dimensional steady normalized Oseenlets given by Chadwick⁵ as

$$\begin{aligned} u_{i1}^0 &= \frac{1}{2\pi} \left\{ \left[\ln r + e^{kx_1} K_0(kr) \right]_{,i} - 2ke^{kx_1} K_0(kr) \delta_{i1} \right\} \\ u_{i2}^0 &= \frac{1}{2\pi} \varepsilon_{ij3} \left[\ln r + e^{kx_1} K_0(kr) \right]_{,j}, \quad p_k^0 = -\frac{1}{2\pi} [\ln r]_{,k} \end{aligned} \quad (39)$$

where p_k^0 is the pressure of the k th Oseenlet. Dang and Chadwick¹⁸ consider this Boundary Element scheme with collocation point weighting functions, linear shape functions, and logarithmic numerical replacement of the singularity $u_{ij}^s = \frac{k}{2\pi} \ln r \delta_{ij}$ by its analytic evaluation. The drag coefficient, given by

$$C_D \approx \int_{\partial\Sigma_B} N_\beta F_{\beta 1} d\sigma \quad (40)$$

is then evaluated and compared against other methods, see figure 2. For this range of Reynolds number, the new method is closer to experiment than the analyses of Kaplun⁶ (asymptotic matching of near-field and far-field representations of the flow at low Reynolds number), Lamb¹⁹ (approximating the form of the Oseen solution), Stokes (slow flow approximation without the treatment of Stokes's paradox), and Tomokita²⁰ (deploying an expansion formula based on an *ad hoc* use of a distribution of simple solutions in Oseen and Euler flow). From existing theory, this is unexpected because, classically, Oseen flow is valid when the linearization to a uniform flow field holds. Such an assumption is violated close to the circular cylinder and is true only in the far field. However, from this new theory, it is expected, as the Oseenlet is a leading order linearization of the NSlet. The results given in Figure 2 demonstrate good agreement with experiment which therefore supports the theory.

2. High Reynolds number flow

In the high Reynolds number limit, it is shown in Chadwick⁵ that the NSlet u_{ik} approximates to the Eulerlet u_{ik}^E given by

$$u_{i1}^E = \frac{1}{2\pi} [\ln r]_{,i} - H(x_1) \delta(x_2) \delta_{i1}, \quad u_{i2}^E = -\frac{1}{2\pi} [\theta]_{,i} \quad (41)$$

where $H(x_1)$ is the heaviside function and θ is the polar angle. Therefore, for high Reynolds number flow (25) becomes

$$u_k \approx u_k^E = \int_{\partial\Sigma_B} F_i^E u_{ik}^E d\sigma' \quad (42)$$

where u_k^E is the Euler velocity generated by an integral distribution of Eulerlets given by u_{ik}^E with strength F_i^E . Equation (42) is also given in Chadwick⁵ but by a different derivation involving a matching between near-field Euler flow and far-field Oseen flow. It is shown by Chadwick⁵ that (42) provides an accurate model. As an example, we see a close relation to the pressure distribution over a circular cylinder surface in uniform flow for both sub-critical laminar flow ($Re \sim 10^6$) and turbulent flow ($Re \sim 10^7$), given in Figure 3. The characteristic features of the physics of the flow such as reversal in the pressure gradient at an angle of around 70-80 degrees, and a negative flattened pressure profile in the wake of the cylinder are reproduced. Hence, the theory presented in this paper is consistent with an Eulerlet model and matches well to experiments²¹.

3. Reynolds number 26 and 36

This time, in (25) the NSlets are approximated by Eulerlets in the near-field and Oseenlets in the far-field, and the two flows are merged for a smooth transition (within the radius range $1 \leq r \leq 6$ such that at $r = 1$ the flow is purely Euler and at $r = 6$ the flow is purely Oseen). A cosine distribution of Eulerlets is considered. Even though the theoretical approach is markedly different, it is equivalent to the description given by Chadwick et al¹² considering a near-field Euler flow matched to a far-field Oseen flow. From this, the following results are then obtained for laminar flow at Reynolds number 26 given in Figure 4, and 36 given in Figure 5. Comparing the flow fields in Figure 4, we note that the separation point is closely matched, and the size and the shape of the eddies are reproduced. Therefore it is seen that, given the approximations made, good agreement is obtained with experiment.

We also present experimental results for the far-field decay at Reynolds number $Re = 36$ from Kovasznay²². Comparing the wake cross-sections with the theory, we note that the trend in diffusion is captured, the general wake profile is captured, and so there is again good agreement.

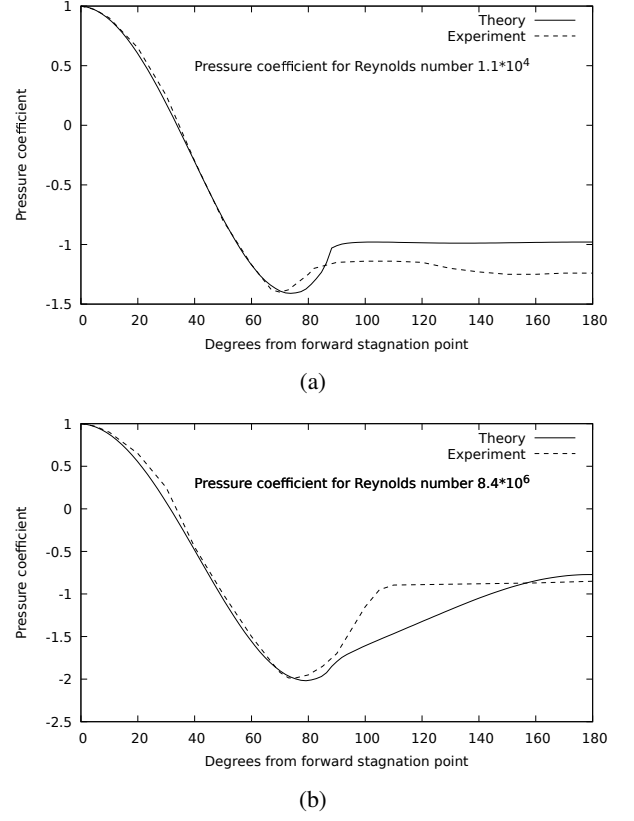


FIG. 3: Pressure distribution comparison between the theory of Chadwick⁵ and the experiment reproduced from the work of Batchelor²¹ (a) for sub-critical laminar flow (b) for turbulent flow.

B. Two-dimensional steady flow past a slender body with elliptical cross-section at high Reynolds number

This case is a reproduction of previous work¹³ on Oseen flow theory. At high Reynolds number close to the body, Oseen flow theory is seemingly inconsistent because of the requirement to satisfy the body boundary condition. Despite this, the Oseen theory appears to be a significant improvement over inviscid flow slender body theory²³ and over Jorgensen's theory²⁴, see Figure 6. The experiments for this comparison were conducted in a low speed wind tunnel at Reynolds number of around $Re = 10^6$. The new theory presented in this paper explains why this should be the case: the Oseenlet is the leading order approximation to the NSlet, and so substituting into (25) gives Oseen flow such that

$$u_k = \int_{\partial\Sigma_B} F_i u_{ik} d\sigma' \approx \int_{\partial\Sigma_B} F_i^0 u_{ik}^0 d\sigma' = u_k^0. \quad (43)$$

Furthermore, in the high Reynolds number limit, the Oseenlet tends towards the Eulerlet, in addition we have

$$u_k^0 = \int_{\partial\Sigma_B} F_i^0 u_{ik}^0 d\sigma' \approx \int_{\partial\Sigma_B} F_i^E u_{ik}^E d\sigma' = u_k^E. \quad (44)$$

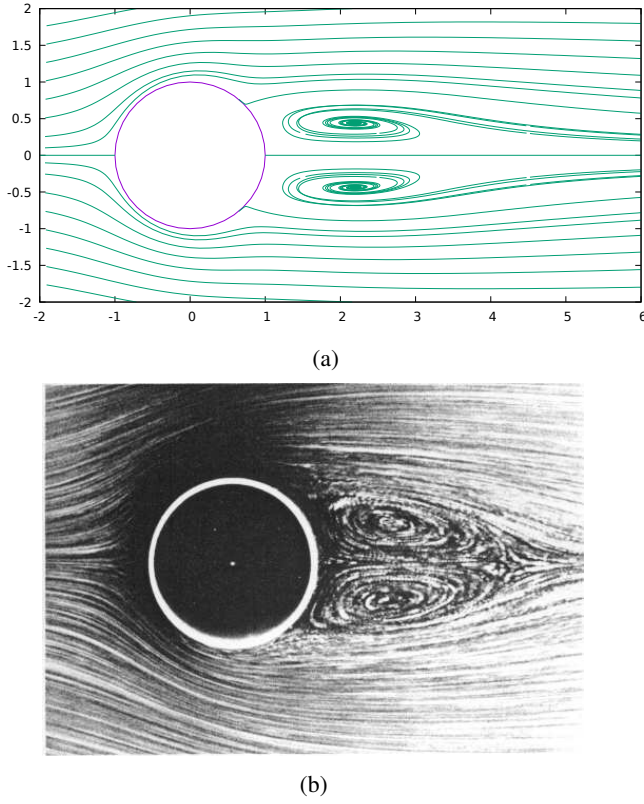


FIG. 4: The streamline flow around a steady two-dimensional circular cylinder at Reynolds number $Re = 26$. (a) Calculation from the theory of Chadwick et al¹². (b) An image from experiment belonging to the estate of Professor Sadatoshi Taneda and reproduced with kind permission from Dr. Hiroshi Taneda

Figure 6 shows that the slender body theory in Oseen flow¹³ gives a close match to experiment for the lift L . Here, ellipticity e is defined as the ratio of the semi-minor axis to the semi-major axis s of the ellipse cross-section and α is the angle of attack. Again, from existing theory this is surprising as the Oseen flow approximation is violated on the surface of the slender body. However, from this new theory it is expected as the Oseenlet is a leading order linearization of the NSlet.

C. Boundary layer flow past a semi-infinite flat plate

In this section, we introduce new theory to describe the Green's function fundamental solution in boundary layer flow, and we call this new function the BL-let. This is then used to describe the flow by applying the boundary layer approximation and considering terms in equation (33). We begin by considering only the first term in (33). However, it is seen that this is not accurate in describing the flow, and so two more subsequent terms are included. Following the method of Kusunaka¹⁴ it is shown that an accurate description is obtained.

In the boundary layer, the Navier-Stokes equations approx-

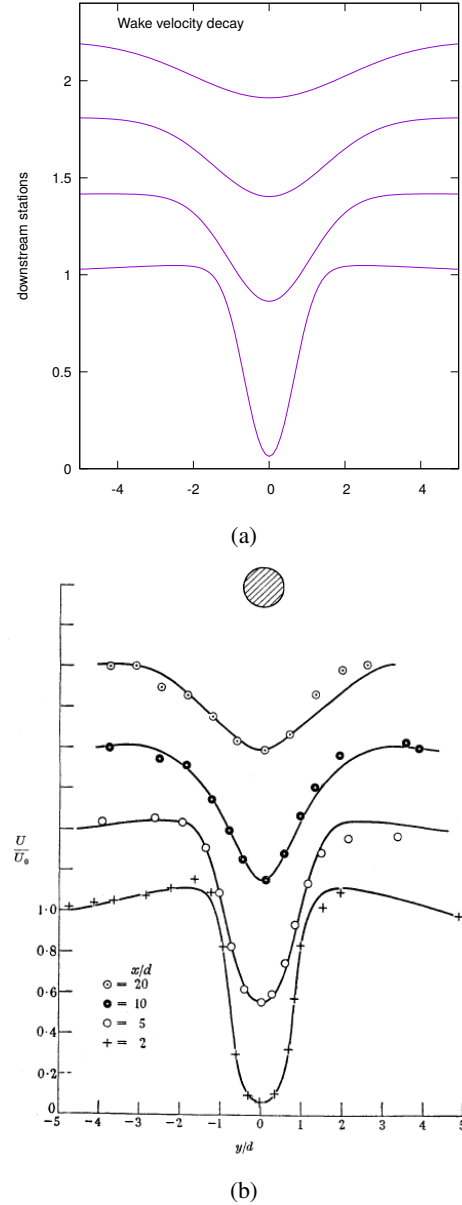


FIG. 5: Axial wake velocity for flow around a steady two-dimensional circular cylinder at Reynolds number $Re = 36$, taken at downstream wake cross-sections positioned at distances 2, 5, 10 and 20 times the diameter. (a) Calculated from the theory of Chadwick et al¹². (b) Reproduced from the experiments of Kovanszay²².

imate to the boundary layer equations²⁵ given by

$$v_j v_{1,j} + v_{1,1} - (1/Re)v_{1,22} = 0 \quad (45)$$

where v_i is the boundary layer velocity. Therefore, the approximation to the NSlet in the boundary layer satisfies

$$v_j v_{11,j} + v_{11,1} - (1/Re)v_{11,22} = -\delta \quad (46)$$

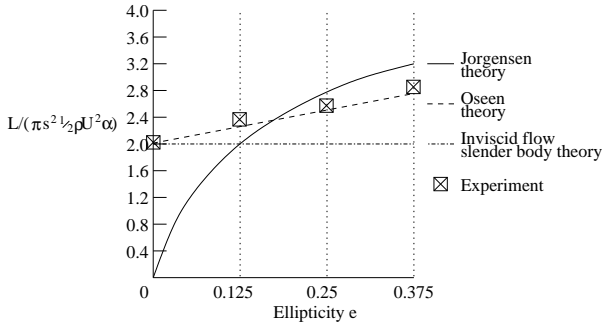


FIG. 6: Comparison of lift between Oseen theory, inviscid potential flow theory and Jorgensen theory against experiment for slender body with elliptic cross-section¹³.

where v_{jk} is the BL-let. So, in the boundary layer, (25) becomes

$$u_k \approx v_k = \int_{\partial\Sigma_B} G_i v_{ik} d\sigma', \quad (47)$$

where G_i is an approximation of the force distribution F_i in the boundary layer. The body boundary lies along the infinite half line, and the symmetry of the problem means that there is only an axial force so that

$$v_k = \int_0^\infty G_1 v_{1k} dx'_1. \quad (48)$$

We now seek v_{ik} by first looking at the leading-order description.

1. Leading-order term

Consider the leading order term in (33), which is the Oseen approximation to the boundary layer Green's function solution, given by

$$v_{11,1}^0 - (1/Re)v_{11,22}^0 = -\delta. \quad (49)$$

We can use Fourier Transforms to evaluate this. Integrating through (49) with the Fourier integral for both the x_1 and x_2 variables gives

$$\begin{aligned} & \int_{-\infty}^{\infty} \int_{-\infty}^{\infty} (v_{11,1}^0 - (1/Re)v_{11,22}^0) e^{-i\omega_1 x_1} e^{-i\omega_2 x_2} dx_1 dx_2 \\ &= - \int_{-\infty}^{\infty} \int_{-\infty}^{\infty} \delta(x_1) \delta(x_2) e^{-i\omega_1 x_1} e^{-i\omega_2 x_2} dx_1 dx_2 = -1 \end{aligned} \quad (50)$$

for the Fourier Transform variables ω_1 and ω_2 . So using standard Fourier Transform theory for differentials, we have

$$i\omega_1 \bar{v} - (1/Re)(i\omega_2)^2 \bar{v} = 1 \quad (51)$$

where \bar{v} is the double Fourier Transform of v_{11} . Therefore,

$$\bar{v} = -\frac{1}{(\omega_2^2/Re) + i\omega_1}. \quad (52)$$

Using the inverse transform $F^{-1}\{1/(a + i\omega_1)\} = H(x_1)e^{-ax_1}$ then gives the single Fourier Transform of v_{11} , \bar{v} , to be

$$\bar{v} = -H(x_1)e^{-\omega_2^2 x_1 / (Re)}. \quad (53)$$

Applying a second inverse transform

$F^{-1}\{1/\sqrt{2ae^{-\omega_2^2/(4a)}}\} = \frac{e^{-\omega_2^2}}{\sqrt{2\pi}}$ then gives

$$v_{11}^0 = -\frac{H(x_1)}{\sqrt{2\pi}} \sqrt{\frac{Re}{2x_1}} e^{-\eta^2} \quad (54)$$

where $\eta = \sqrt{\frac{Re}{4x_1}}x_2$ is the boundary layer variable. Since $v_{11}^0 = \Psi_{,2}^0$, the streamfunction is

$$\begin{aligned} \Psi^0 &= -\frac{Re}{4\pi x_1} \int_0^{x_2} e^{-\eta^2} dx'_2 = -\frac{1}{\sqrt{\pi}} \int_0^\eta e^{-\eta'^2} d\eta' \\ &= -(1/2)\text{erf}\eta. \end{aligned} \quad (55)$$

From (48), we then have for the x_1 component of velocity

$$v_1^0 = \int_0^\infty G_1^0 v_1^0 dx'_1 = \int_0^{x_1} G_1^0 \Psi_{,2}^0 dx'_1 \quad (56)$$

where G_1^0 is the leading-order approximation of the force distribution G_1 and v_1^0 is the leading-order component of the boundary layer velocity. Therefore, the streamfunction Ψ^0 for this flow is given by

$$\Psi^0 = \int_0^{x_1} G_1^0 \Psi^0 dx'_1 = \int_0^{x_1} G_1^0 (-(1/2)\text{erf}\eta^*) dx'_1 \quad (57)$$

where $\eta^* = \sqrt{\frac{Re}{4x_1^*}}x_2$, $x_1^* = x_1 - x'_1$. The variable change $q = x'_1/x_1$ gives

$$\Psi^0 = x_1 \int_0^1 G_1^0(x_1 q) (-(1/2)\text{erf}(\eta/\sqrt{1-q})) dq. \quad (58)$$

However, we know²⁵ from the self-similarity of the problem given in the standard Blasius approach that $\Psi^0 = \sqrt{x_1}f(\eta)$ for some function $f(\eta)$. Therefore, to get the appropriate variation in x_1 , it must be that $G_1^0(x_1) = a/\sqrt{x_1}$ for some constant a . So,

$$\Psi^0 = \int_0^{x_1} (a/\sqrt{x'_1}) (-(1/2)\text{erf}\eta^*) dx'_1. \quad (59)$$

From this result, an expression for the x_2 component of velocity can be calculated. Differentiating (59) with respect to x_1 gives

$$\begin{aligned} v_2^0 &= -\Psi_{,1}^0 = (a/\sqrt{x_1})((1/2)\text{erf}(\infty)) \\ &\quad - \int_0^{x_1} (a/\sqrt{x'_1}) (-(1/2)\text{erf}\eta^*)_{,1} dx'_1 \\ &= (1/2)(a/\sqrt{x_1}) - (1/2) \int_0^{x_1} (a/\sqrt{x'_1}) (\text{erf}\eta^*)_{,1} dx'_1 \\ &= (1/2)(a/\sqrt{x_1}) - (1/2) \int_\eta^\infty (a/\sqrt{x'_1}) (\text{erf}\eta^*)_{,\eta^*} d\eta^*. \end{aligned} \quad (60)$$

Here, for a function $f(x_1 - x'_1)$, we have defined $f_{,1'} = \frac{\partial f}{\partial x'_1}$, and so $f_{,1'} = -f_{,1}$. Now consider the variable $q^2 = \eta^{*2} - \eta^2$, then $q/\eta^* = \sqrt{x'_1}/\sqrt{x_1}$ and $d\eta^* = \sqrt{x'_1}/\sqrt{x_1}dq$, giving

$$\begin{aligned} v_2^0 &= (1/2)(a/\sqrt{x_1}) - (1/2)(a/\sqrt{x_1}) \int_0^\infty \frac{2}{\sqrt{\pi}} e^{-\eta^{*2}} dq \\ &= \frac{a}{2\sqrt{x_1}}(1 - e^{-\eta^2}). \end{aligned} \quad (61)$$

To find v_1^0 , recall that this velocity satisfies

$$v_{1,1}^0 - (1/Re)v_{1,22}^0 = 0, \quad (62)$$

from the continuity equation, $v_{1,1}^0 = -v_{2,2}^0$. Substituting into (62) and integrating with respect to x_2 whilst ensuring that the solution decays, gives

$$v_1^0 = \sqrt{Re} \frac{\sqrt{\pi}}{2} a (\operatorname{erf} \eta - 1). \quad (63)$$

The boundary condition on the flat plate is that $v_1^0 = -1$, and so $a = \frac{\sqrt{2}}{\sqrt{(Re)\pi}}$ giving

$$v_1^0 = \operatorname{erf} \eta - 1, \quad (64)$$

and therefore

$$v_2^0 = \frac{(1 - e^{-\eta^2})}{\sqrt{(Re)\pi x_1}}. \quad (65)$$

This solution is well-known because it has also been calculated by an entirely different method by Burgers²⁶ and is called the Oseen-Blasius solution. For comparison, Burgers' method is given in the Appendix A. Unfortunately, this solution gives a large discrepancy for the stress and so is not sufficiently accurate to be useful. However, the expectation is that if more terms in the expansion for the NSlet given by equation (33) are considered, then there will be greater accuracy. So, to enable a more accurate description we consider additional terms in the expansion.

2. Higher-accuracy description

Consider further terms in the velocity expansion of the boundary layer Green's function BL-let

$$v_{ik} = v_{ik}^0 + v_{ik}^I + v_{ik}^{II} + \dots \quad (66)$$

Substituting into (46) then gives

$$\begin{aligned} &(v_{j1}^0 + v_{j1}^I + v_{j1}^{II} + \dots)(v_{i1,j}^0 + v_{i1,j}^I + v_{i1,j}^{II} + \dots) + \\ &v_{11,1}^0 + v_{11,1}^I + v_{11,1}^{II} + \dots \\ &- (1/Re)(v_{11,22}^0 + v_{11,22}^I + v_{11,22}^{II} + \dots) \\ &= -\delta. \end{aligned} \quad (67)$$

Rearrange such that

$$\begin{aligned} v_{11,1}^0 - (1/Re)v_{11,22}^0 &= -\delta \\ v_{11,1}^I - (1/Re)v_{11,22}^I &= -v_{j1}^0 v_{11,j}^0 \\ v_{11,1}^{II} - (1/Re)v_{11,22}^{II} &= -v_{j1}^0 v_{11,j}^I - v_{j1}^I v_{11,j}^0 \\ v_{11,1}^{N-1} - (1/Re)v_{11,22}^{N-1} &= -\sum_{I=0}^{N-2} v_{j1}^I v_{11,j}^{N-1-2}. \end{aligned} \quad (68)$$

Considering M terms in the expansion, and integrating (68) such that

$$v_1^N = \int_0^{x_1} G_1^M v_{11}^N dx'_1 \quad (69)$$

gives

$$\begin{aligned} v_{1,1}^0 - (1/Re)v_{1,22}^0 &= 0 \\ v_{1,1}^I - (1/Re)v_{1,22}^I &= -\int_0^{x_1} G_1^M v_{j1}^0 v_{11,j}^0 dx'_1 \\ v_{1,1}^{II} - (1/Re)v_{1,22}^{II} &= -\int_0^{x_1} G_1^M (v_{j1}^0 v_{11,j}^I - v_{j1}^I v_{11,j}^0) dx'_1 \\ v_{1,1}^{N-1} - (1/Re)v_{1,22}^{N-1} &= -\int_0^{x_1} G_1^M \sum_{I=0}^{N-2} v_{j1}^I v_{11,j}^{N-1-2} dx'_1. \end{aligned} \quad (70)$$

Integrating (66) in the same way gives

$$v_k = v_k^0 + v_k^I + v_k^{II} + \dots \quad (71)$$

Substituting this expansion into (45) gives

$$\begin{aligned} &(v_j^0 + v_j^I + v_j^{II} + \dots)(v_{i,j}^0 + v_{i,j}^I + v_{i,j}^{II} + \dots) + \\ &v_{1,1}^0 + v_{1,1}^I + v_{1,1}^{II} + \dots \\ &- (1/Re)(v_{1,22}^0 + v_{1,22}^I + v_{1,22}^{II} + \dots) \\ &= -\delta. \end{aligned} \quad (72)$$

Rearranging gives

$$\begin{aligned} v_{1,1}^0 - (1/Re)v_{1,22}^0 &= 0 \\ v_{1,1}^I - (1/Re)v_{1,22}^I &= -v_j^0 v_{1,j}^0 \\ v_{1,1}^{II} - (1/Re)v_{1,22}^{II} &= -v_j^0 v_{1,j}^I - v_j^I v_{1,j}^0 \\ v_{1,1}^{N-1} - (1/Re)v_{1,22}^{N-1} &= -\sum_{I=0}^{N-2} v_j^I v_{1,j}^{N-1-2}. \end{aligned} \quad (73)$$

Comparing (70) and (73), the left hand side of each equation is the same and so the right hand sides of each must equal each other.

It is seen that (73) is identical to the expansion given by Kusunaka et al¹⁴ who finds the first three terms. These terms indicate that the expansion converges towards the exact boundary layer solution. However, Kusunaka et al obtain their iteration method by considering an Oseen linearization of the flow field. Whilst this will hold in the far-boundary-layer close to the uniform stream, there is no evidence that it will converge to the boundary layer solution throughout the flow field. Therefore, there is no theoretical justification from

Kusukawa that the expansion holds close to the boundary. Instead, we see that from the theory presented here, there is an expectation that the iteration method will converge to the exact boundary layer solution, and the numerical results reproduced from¹⁴ in Figure 7 indicate this.

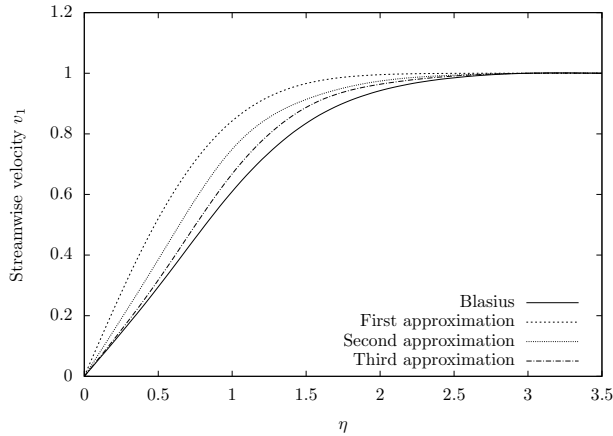


FIG. 7: The boundary layer velocity calculated from various approximations to the boundary layer Green’s function given by Kusukawa¹⁴

VI. CONCLUSION

A new method is given which represents the incompressible Navier-Stokes velocity by a linear Boundary Integral distribution of Navier-Stokes Green’s functions which we call NSlets for both the steady and unsteady problem in two- and three-dimensional flow. The NSlets are determined and given in terms of an infinite series with the first term being the respective Oseenlets.

The representation is the same for both exterior and interior flow problems. The strength of the NSlets is given by the stress tensor and so is the fluid force acting on the boundary. In the near-field for low Reynolds number, the NSlets tend towards Stokeslets and so the Stokes flow velocity representation^{2,3} is recovered. Similarly, for Oseen flow, the NSlets become Oseenlets and the Oseen flow velocity representation^{4,15} is recovered. In the high Reynolds number limit, the NSlets tend towards Eulerlets and the Euler flow velocity representation⁵ is recovered.

Given this representation, a problem which stipulates the velocity on the body boundary is then easily solved in a straightforward manner, in the same way as for Oseen and Stokes flow problems. Once the velocity is found, then the solution can be put back into the equations in order to determine the pressure. Therefore, this represents a general linearized solution to the incompressible Navier-Stokes problem by a Green’s integral distribution of Green’s functions.

Three two-dimensional benchmark problems are considered, uniform flow past a circular cylinder, a slender body with elliptical cross-section, and a semi-infinite flat plate. For the

first two problems, the first term (Oseenlet) is given to approximate the NSlet. For high Reynolds number, this is further approximated by the Eulerlet. For the final problem, the first three terms are considered and the boundary layer approximation is applied. For all cases, good agreement with benchmark results are found.

This gives explanation to Shankar’s observation² that the Oseen flow representation is a surprisingly good model given the body boundary condition violation. The explanation is that the fluid velocity is represented by an integral distribution of NSlets and the leading order approximation to the NSlet is the Oseenlet, so an Oseen flow model is a leading order representation of the flow for these problems.

Future work is to model applications across the Reynolds number range by developing a Boundary Element code for this Boundary Integral representation. Rather than using the first few terms in the expansion for the NSlets, a numerical scheme will be used to determine more accurately the full NSlet which can then be fed into the Boundary Element code.

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Appendix A: Burgers boundary layer approach

We follow the method of Burgers²⁶ who assumes Oseen flow in the boundary layer by an axial distribution of Oseenlets given by

$$u_k \approx u_k^0 = \int_0^\infty F_1^0 u_{1k}^0 dx'_1, \quad (\text{A.1})$$

where F_1^0 is the strength of the drag Oseenlets $u_{k1}^0 = u_{1k}^0$ lying along the positive x_1 axis. This representation has been considered by Olmstead⁴ who finds a solution by using the Wiener-Hopf technique²⁷. However, Olmstead omits a few key proofs and a complete detailed analysis is given in Darghoth²⁸. The Wiener-Hopf technique then gives the force distribution as

$$F_1^0 = \frac{2}{\sqrt{(Re)\pi x_1}}. \quad (\text{A.2})$$

In the boundary layer, this can be further approximated. Letting the ratio of x_1/x_2 become large in the downstream bound-

ary layer, Adamu and Chadwick²⁹ show that the drag Oseenlet approximates to Imai's far-field drag expression³⁰. Equivalently, Burgers²⁶ also approximates the Oseenlet, and in both cases the solution in the boundary layer is given by

$$\begin{aligned} u_{11}^0 &\approx v_{11}^0 = \psi_{,2}^0 \\ u_{21}^0 &\approx v_{21}^0 = -\psi_{,1}^0 \\ \psi^0 &= -(1/2)\text{erf}\eta + (1/(2\pi))\theta, \end{aligned} \quad (\text{A.3})$$

where $\eta = \sqrt{Re/(4x_1)x_2}$ is the boundary layer variable and θ is the polar angle. (We note in this formulation the term $(1/(2\pi))\theta$ is required in the representation of ψ^0 whereas in the derivation in Section V C it is not. This is because here we give the velocity v_2^0 representation first directly from the integral (A.4) given next, whereas in Section V C we give the streamfunction Ψ^0 representation first for which the term $(1/(2\pi))\theta$ is lower order and so can be ignored. The velocity v_2^0 is then determined from this.) Substituting this into (A.1) gives an expression for the transverse boundary layer velocity component v_2^0 as

$$u_2^0 \approx v_2^0 = \int_0^\infty F_1^0 v_{21}^0 dx'_1. \quad (\text{A.4})$$

The term $(1/(2\pi))\theta$ in ψ^0 from equation (A.3) represents a line of two-dimensional Laplacian sources, and an integral distribution of these with strength given by (A.2) is given, for example, in Darghoth²⁸. By using the substitutions for the integral variable from x'_1 to η^* where $\eta^* = \sqrt{\frac{Re}{4x_1^*}}x_2$, $x_1^* = x_1 - x'_1$, and then to q where $q^2 = \eta^{*2} - \eta^2$, the integral in (A.4) is calculated, see Burgers²⁶ and Darghoth²⁸. This gives

$$v_2^0 = \frac{(1 - e^{-\eta^2})}{\sqrt{(Re)\pi x_1}}. \quad (\text{A.5})$$

From this, the axial streamwise velocity can be calculated, for example in the same way as given in Section V C.